



## Eulerian Lagrangian Simulation of Particle Capture and Dendrite Formation on Binary Fibers

S. Akbarnezhad<sup>\*a</sup>, A. Soltani Goharrizi<sup>a</sup> M. Salmanzadeh<sup>b</sup>

<sup>a</sup>Department of Chemical Engineering, Shahid Bahonar University of Kerman, Kerman, Iran

<sup>b</sup>Department of Mechanical Engineering, Shahid Bahonar University of Kerman, Kerman, Iran

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### ABSTRACT

The capture efficiency of the small aerosol particle is strongly influenced by the structure of fibrous layers. This study presents particle deposition and dendrite formation on different arrangements of binary fibers. 2-D numerical simulation is performed using the open source software of OpenFOAM. In the instantaneous filtration of a single fiber, obtained results are in good agreement with the existing model. Results showed that addition of nanofiber to microfiber led to high capture efficiency for the particle size 50nm at the cross arrangement with fibers distance 2 $\mu$ m. When particle gets larger, i.e. 150 nm, binary fibers have higher capture efficiency and pressure drop than the single microfiber at all arrangements, especially for the fibers distance 1.5  $\mu$ m. Therefore, the good fibers arrangement here seems the cross arrangement with the high capture efficiency, average pressure drop and fibers distance 2  $\mu$ m.

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### NOMENCLATURE

$C_D$	Drag coefficient	$Re_p$	Reynolds number of particle
$d_{fm}$	Diameter of microfiber	$St = \rho_p d_p^2 C_c V / 18\mu d_f$	Stokes number
$d_{fn}$	Diameter of nanofiber	$T$	Temperature
$d_p$	Particle diameter	$U$	Fluid velocity
$E$	Efficiency of loaded filter	$U_p$	Particle velocity
$E_0$	Efficiency of clean filter	<b>Greek Symbols</b>	
$F_B$	Brownian force	$\alpha$	Solid volume fraction or SVF
$F_D$	Drag force	$\gamma$	Kinematic viscosity
$k_B$	Boltzmann constant	$\lambda$	Mean free path
$k_{pp}$	Permeability constant (m <sup>2</sup> )	$\mu$	Dynamic viscosity
$l$	Fiber length	$\rho$	Density of fluid
$M$	Mass of loaded particle per fiber volume	$\rho_p$	Density of particle
$m_p$	Mass of particle	$\omega$	Occupied volume fraction of cell by particle
$P$	Pressure		

### 1. INTRODUCTION

The motion and deposition of particle phenomena can be seen in many fields such as, environment, energy and chemical industry [1]. Separation of the small particle is

an important challenge for researcher due to great concern for human health and the environment risks [2-4]. Filtration is an effective technique for removing small particles from the fluid because of being easy to use, inexpensive and high collection efficiency.

Real fibrous filters are composed of fibers that they are randomly oriented in contrast with perpendicular the plane as supposed in the theoretical models. The fabric

\*Corresponding Author's Email: sh.akbarnezhad@eng.uk.ac.ir (S. Akbarnezhad)

filter is widely applied due to its convenient, simple and general features [5]. Current researches in field of fabric filters focused on the filtering mechanisms, efficiency and pressure drop [5]. The base of the classic filtration theories is formed with Single fiber efficiency (SFE), which defines the efficiency of a single fiber that is placed in a cell [6]. Three mainly mechanisms are considered for the particle capture by filtration; impaction, interception and Brownian diffusion [7]. The efficiency of a fiber obtain the sum of the efficiencies from each individual mechanisms [8]. A variety of semi-empirical expression are developed for predicting the efficiency and pressure drop of filters. These expressions are made for clean filters in initial time of filtration [6, 9-11]. However, since the filtration process keeps on for a long time, the filter doesn't remain clean during the particle loading time. Particles deposit on the fibers and form the dendrite structures with complicated geometries. These structure have eligible effect on the efficiency and pressure drop of the filter. A preliminary model for dendrite formation was developed at particle capture mechanism of interception by Payatakes and Tien [12]. Later, this model improved and extended for impaction and Brownian diffusion mechanisms [13, 14], where the effect of dendrite formation on the flow field was not assumed. Kanaoka et al. [15] simulated the dendrite structure on a single fiber by the Monte-Carlo technique in a Kuwabara cell. They presented a linear formula for SFE of a loaded fiber to clean fiber as mass loaded on the fiber at interception regime. However, no recalculating of flow field was considered during dendrite growth. Filippova and Hanel [16] and Lantermann and Hanel [17] also considered the flow field recalculation in their studies. Also, Hosseini and Tafreshi [18] simulated the 3-D dendrite formation on a single fiber using the ANSYS-Fluent CFD code. They presented a methodology, which is used during instantaneous particle loading, to explain the effect of the different capture mechanisms on the filter performance. Furthermore, the necessary condition for recalculation of the flow filed was that the total volume of deposited particles to be close to 5 % of the fiber volume [18]. Rafał Przekop and Leon Gradoń [19] modeled the deep bed filtration considering the effect of particle growth on the filter structure and flow field. Their model was able to predict the dynamic filter behavior during instantaneous particle loading.

Moreover to the particle capture mechanisms, other parameters such as, filter structure, solid volume fraction (SVF), filter thickness, the microstructure of disordered fibers in fibrous materials, filtration velocities and fiber diameters can also be effective on the filter performance and the particle capture process [20-22]. Wang et al. [23] simulated the effect of different fiber arrangements on the capture efficiency and pressure drop of multi-layer fiber filters where

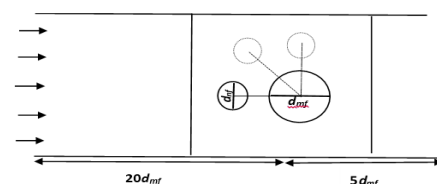
fibers were of the same size. Their results showed that the staggered model of fibers has higher capture efficiency than the parallel model. In order to find the influence of the fiber diameter dissimilarity on the performance of a bimodal filter, Fotovati et al. [24] performed numerical simulations and utilized a unimodal equivalent diameter for the bimodal filter media. Particle deposition and filtration performance of a bilayer filter composed of a nanofibrous front layer and a microfibrinous backing layer were numerically studied by Przekop and Gradoń [21].

The experimental results of Podgorski et al. [25] showed that the capture efficiency of the small aerosol particle is strongly influenced by the structure of nanofibrous layers. Since the nature of fibrous filters causes a difficulty to investigate the details of particle deposition and dendrite formation, it offers to follow numerical simulation of the filtration process than experiments.

The present study investigates the influence of the binary system of the nano- and microfiber on small aerosol particles captured and dendrite formation (particle size 50 nm and 150 nm). The simulation is performed using open source software of OpenFOAM. Here, it is utilized a methodology for particle deposition and growth during instantaneous particle loading. The icoLagrangianFoam solver of OpenFOAM 2.2.0 is extended for simulation of the particle capture and dendrite formation on binary fibers surface. The effects of fibers arrangement and distance between fibers on the capture efficiency, pressure drop and dendrite formation of particles are investigated.

## 2. NUMERICAL SIMULATION

**2. 1. Problem Description** Figure 1 shows an example of the 2-D computational box, which consists of two fibers with different diameter 500 nm and 2  $\mu\text{m}$ . A square medium is considered around of fibers as a solid volume fraction of filter medium [18]. For having developed flow the entrance of filtration medium, inlet length of channel is considered bigger than outlet length. Aerosol particles with diameter of 50 and 150 nm are injected randomly through inlet patch to the system. The air flow of system assumes to be laminar and incompressible with constant density,  $\rho$  and viscosity,  $\mu$ .



**Figure 1.** Schematic diagram of the simulation domain

**2. 2. Equation of Motion** In this study, Eulerian and Lagrangian approaches are used to compute the fluid flow and particle phase equations, respectively. Since the volume fraction of particles in the continuous phase is less 12 %, the particle-particle interaction and particle influence on continuous phase is ignored [26]. Particles are randomly injected with positions along the inlet boundary, which is set so as to control the inlet particle concentration (particle number 4000/s). The one way coupling approach is applied for 2-D continuity and momentum equations are solved for gas phase stated as follows [27]:

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0 \quad (1)$$

$$\rho \left( U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} \right) = -\frac{\partial P}{\partial x} + \mu \left( \frac{\partial^2 U}{\partial x^2} + \frac{\partial^2 U}{\partial y^2} \right) + \frac{\mu \varphi}{k_{pp}} U \quad (2)$$

$$\rho \left( U \frac{\partial V}{\partial x} + V \frac{\partial V}{\partial y} \right) = -\frac{\partial P}{\partial y} + \mu \left( \frac{\partial^2 V}{\partial x^2} + \frac{\partial^2 V}{\partial y^2} \right) + \rho g_y + \frac{\mu \varphi}{k_{pp}} V \quad (3)$$

In the simulation strategy used in this study, the inlet velocity is considered to be 0.001 m/s. Furthermore, it is assumed that the continuum flow is dominant with microfiber diameter 2  $\mu\text{m}$ . Moreover, symmetry boundary conditions are used for the sides of the channel. The reason for this boundary condition is to prevent net flows in lateral sides [28]. Also the air flow enters the computational domain through inlet velocity and leaves through boundary condition of the outlet pressure, respectively. The no-slip boundary condition is used on the wall of fibers.

The computations are performed using the extended solver of icoLagrangianFoam with an unstructured mesh around the fibers to solve for two-dimensional flow. The grid number around the nano- and microfiber was 12 and 40 after grid independence test, respectively. This test is done on the pressure drop of the net air flow in binary fibers with the horizontal arrangement (Table 1). There are many different numerical schemes in the OpenFOAM which can be applied to discrete the continuity, momentum and particle equations. In this study, the finite volume method based on the PISO algorithm for pressure-velocity coupling is used. The numerical discrete schemes are chosen as follows: the convection terms with the Gauss cubic scheme, the Laplacian term with the Gauss linear corrected scheme, the gradient of pressure term with the Gauss vanleer

**TABLE 1.** Grid independence test on the pressure drop of binary fibers

Grid number around the microfiber	15	20	30	40	50
Grid number around the nanofiber	10	10	12	12	12
$\Delta P$ (Pa)	0.228	0.227	0.203	0.195	0.195

scheme and also the derivative of time with the Euler implicit scheme.

**2. 3. Particle Transport Equation** In Lagrangian approach, each particle tracks throughout the solution domain. The particle's position in time obtains by integrating the force balance on a given particle. In this study, the acting forces on particle are drag and Brownian forces. Since particle sizes are considered to be small with diameters 50 and 150 nm, impaction mechanism practically does not exist. Li and Ahmadi [29] concluded the air drag force as a dominant force on the particle when  $Re_p = \rho U d_p / \mu < 1$ . Therefore, the equation of particle motion stated as follows:

$$m_p \frac{dU_p}{dt} = F_D + F_B \quad (4)$$

In this study Particles are assumed to have a spherical shape. Therefore, in OpenFOAM the air drag force for spherical particle is defined as follows [30]:

$$F_D = \frac{3m_p \mu C_D Re_p}{4\rho_p d_p^2} (U - U_p) \quad (5)$$

In Equation (5) the expression for drag coefficient  $C_D$ , is presented in the following form [30]:

$$C_D = \frac{24}{Re_p} \quad Re_p \leq 0.1$$

$$C_D = \frac{24}{Re_p} \left( 1 + \frac{1}{6} Re_p^{\frac{2}{3}} \right) \quad 0.1 \leq Re_p \leq 1000 \quad (6)$$

$$C_D = 0.424 \quad Re_p > 1000$$

where

$$Re_p = \frac{\rho_f d_p |U - U_p|}{\mu_f} \quad (7)$$

Furthermore, Brownian force acting on the particle is described in literature [31]:

$$F_b = G \sqrt{\frac{\pi S_o}{\Delta t}} \quad (8)$$

where G is a vector whose components are independent zero-mean, unit variance Gaussian random numbers [32]. The components of the Brownian force for particles are white noise processes, with spectral intensities described by Equation (8) [32]:

$$S_{ni,j} = S_o \delta_{i,j} \quad (9)$$

$$S_o = \frac{216\gamma k_B T}{\pi^2 \rho d_p^5 \left(\frac{\rho_p}{\rho}\right)^2 c_c} \quad (10)$$

The value of Cunningham correction factor,  $C_c$  and the mean free path,  $\lambda$  are determined using Equations (11) and (12) stated as follows:

$$C_c = 1 + \frac{2\lambda}{d_p} \left( 1.257 + 0.4 \exp\left(-0.55 \left(\frac{d_p}{\lambda}\right)\right) \right) \quad (11)$$

$$\lambda = 0.385 \left( \frac{\rho_p d_p k_B T}{\mu^2 \pi^2} \right)^{1/2} \quad (12)$$

## 2. 4. Particle Tracking Algorithm in OpenFOAM

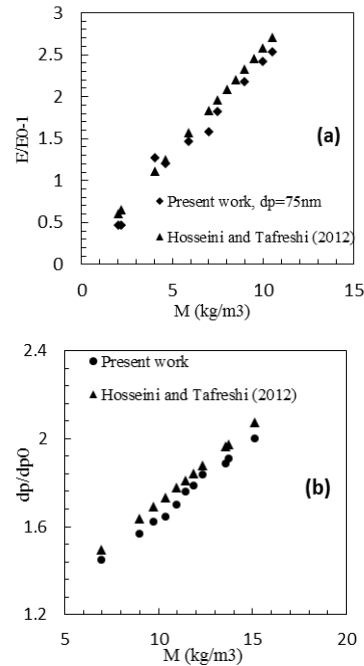
The icolagrangianFoam solver of OpenFOAM is a power algorithm for particle tracking. This algorithm is presented in detail by Macpherson et al. [33] and also in brief by Mead-Hunter et al. [31]. The extended solver for simulating dendrite formation of particle on fiber surface is as follows. First, the algorithm finds all cell of the fiber wall (a boundary face for particle deposition). Then, it starts marking coordinates of occupied cells on the fiber wall from particle. The particle deposit on wall face when the particle distance from wall face or last deposited particle is smaller than particle radius. So deposited particle in the algorithm have no more movement and removes from the particle tracking domain. Then, adding a source term to momentum equation (Equations (2) and (3)) can prevent to flow through these marked cells. Like this source term, Saleh et al. [34] considered a sink term to add momentum equation that causes an artificial pressure drop for the flow when passing through these occupied cells.

## 3. RESULTS AND DISCUSSION

It is necessary to assess the accuracy of the results obtained from the modified Lagrangian approach used in this numerical work. In this section, validation of the particle deposition efficiency (the number of deposited particles to the total number of particles injected into the domain of simulation) and pressure drop is performed by comparing the results with those achieved by Hosseini and Tafreshi [18]. Figure 2 shows the normalized single fiber efficiency  $E$  (the ratio of the average single fiber efficiency  $E$  to the efficiency of clean fiber  $E_0$ ) and pressure drop versus mass of the deposited particles on a fiber. Two recent validations show good agreement with the obtained results from this simulation.

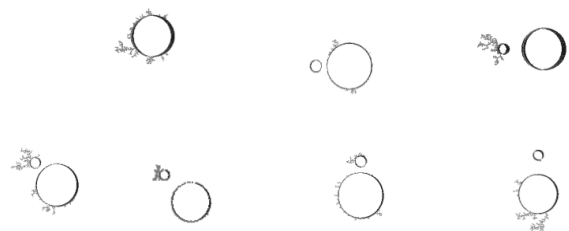
### 3. 1. Deposition Pattern and Dendrite Formation of Different Fibers Arrangement and Distance

The shape of fibers will change during particle loading depending on particle deposition mechanisms. As the Brownian diffusion is dominant, particle trend to form a uniform distribution of the particle deposition and dendrite chain around the fiber. Interception mechanism mainly causes the growth of dendrites on the lateral sides of fiber. Particles deposit in front of fiber when the impaction mechanisms is dominant. In this study, two distances of 1.5 and 2 $\mu\text{m}$  between centers of binary fibers were considered for observing how the particle capture on fiber surfaces.



**Figure 2.** (a) Normalized single fiber efficiency vs. fiber loading  $M$  for a fiber with  $d_f=1 \mu\text{m}$  and  $\alpha = 5\%$ , (b) Normalized pressure drop for a fiber with  $d_f=20\mu\text{m}$  and  $d_p=2\mu\text{m}$ .

Figure 3 shows the particle deposition for the particle size 50 nm on a single fiber and binary fibers in different arrangement and distance. Particles deposit and grow around the binary fibers for three arrangements like the single fiber. In the horizontal arrangement, the nanofiber competes with microfiber to capture particles (top-right). In the other hand, this arrangement is similar to single fiber for the particle deposition and dendrite formation. But the faster dendrite formation on the nanofiber causes these dendrite chains to act as a good collector for the next particle deposition than later microfiber. So, there is a very small dendrite chain around the microfiber, which means that it needs more loading time for having longer dendrite.



**Figure 3.** Deposition pattern and dendrite formation of particle size 50 nm in different fibers arrangement and distance in contrast with a single microfiber.

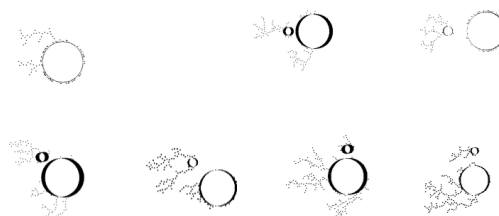
At the vertical arrangement, binary fibers have the same uniform deposition around the fibers (bottom-right). In cross arrangement, binary fibers collect the particle on surfers with a dendrite chains around of fibers. The reason of the more growth of dendrite chains on the nanofiber can be similar to horizontal arrangement (bottom-left). These deposition patterns here have been observed in the other numerical simulation results, which have been done by lattice-Boltzmann method [21, 35]. There is a fairly good agreement in shape of dendrites with reference results. Also, the smaller distance of fibers cause more uniformly growth of particle on fiber surfaces at all fiber arrangements.

Figure 4 presents the effects of the fibers arrangement and distance on the particle deposition upon the interception mechanism. In this subsection, the particle size was considered to be 150nm. Generally, interception mechanism can be dominant for particles in range of 0.1-1 $\mu$ m [35]. It can be seen in Figure 4 that deposition of the particles created dendrite chains close to sides of the single fiber (top-left). This deposition pattern is in qualitative agreement with the observation of Hosseini and Tafreshi [18]. When there is a horizontal arrangement, nanofiber has a shielding effect for the back microfiber and the particle deposit with dendrite chains on its lateral sides clearly (top-right). But for two others cross and vertical arrangements, nano- and microfiber of binary system contribute to capture and form dendrite on surfaces. Also the location of the dendrite chains moves from 45° of microfiber surface to middle of it (bottom-left and right). In fact the faster dendrite formation on nanofiber surface increases the local fluid velocity at the gap domain between fibers. Therefore, here, the Peclet number of particles increases, which means that particles move to stream lines of close to microfiber surface and deposited on surface layer [23].

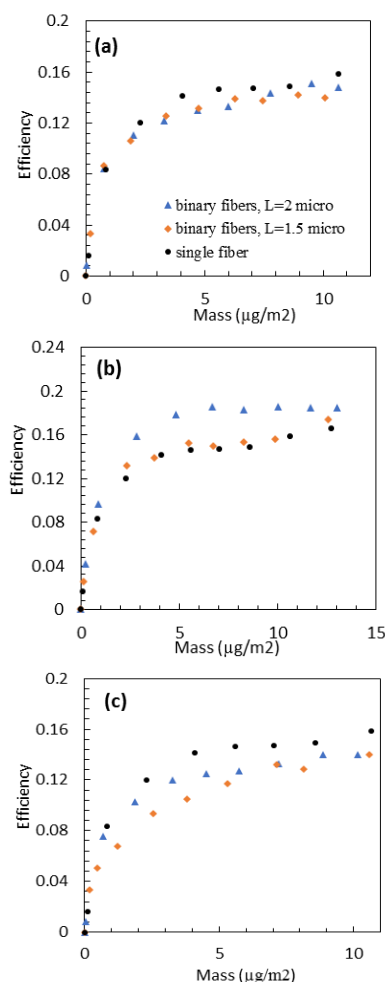
### 3. 2. The Effect of Different Fibers Arrangement and Distance on Capture Efficiency During Particle Loading

Figures 5 and 6 show the capture efficiency of the single fiber and different arrangement and distance of binary fibers as mass loaded for the particle size 50 and 150 nm, respectively. Results indicate that the capture efficiency increase fairly constant with increasing the loaded mass on fiber surfaces at all different arrangements (Figures 5a-c and 6a-c). In this subsection, the fiber distance of 1.5 and 2 $\mu$ m between centers of binary fibers are considered for evaluating the performance of binary fibers arrangement in the particle capturing process. It was concluded that the fibers arrangement and distance have a clear effect on the particle capture efficiency and the pressure drop. In fact, a good arrangement causes a high efficiency and a lower pressure drop. In horizontal arrangement of binary fibers and the particle size 50 nm, capture

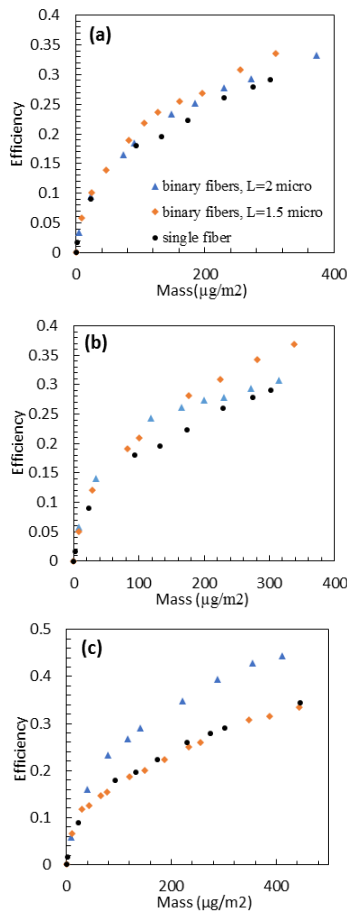
efficiency have a fairly same increasing as mass loaded for two fibers distances. For the cross arrangement, increasing of capture efficiency is higher for fibers distance 2  $\mu$ m. When fibers distance decreases to 1.5  $\mu$ m, the capture efficiency follows a similar trend of the single microfiber efficiency.



**Figure 4.** Deposition pattern and dendrite formation of particle size 150 nm in different fibers arrangement and distance in contrast with a single microfiber.



**Figure 5.** Capture efficiency of different arrangements of binary fibers with fibers distance 1.5 and 2 $\mu$ m as mass loaded for the particle size 50nm (a) the horizontal arrangement, (b) the cross arrangement, (c) the vertical arrangement



**Figure 6** Capture efficiency of different arrangements of binary fibers with fibers distance 1.5 and 2 $\mu$ m as mass loaded for the particle size 150 nm (a) the horizontal arrangement, (b) the cross arrangement, (c) the vertical arrangement

The capture efficiency of single microfiber is higher than binary fibers with different fibers distance in the vertical arrangement.

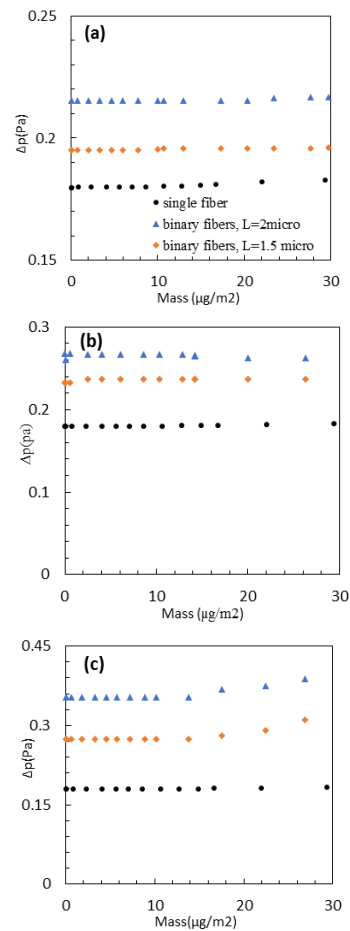
For the particle size 150 nm (Figure 6), binary fibers have higher efficiency at the cross and horizontal arrangements than the single microfiber, especially for smaller fibers distance  $L=1.5 \mu\text{m}$ . In the other hand, in vertical arrangement with fibers distance 1.5  $\mu\text{m}$ , the capture efficiency of binary fibers is equal with the single fiber, but fibers distance 2  $\mu\text{m}$  causes the higher efficiency for binary fibers.

**3. 3. Pressure Drop of Different Fibers Arrangement and Fibers Distance During Particle Loading**

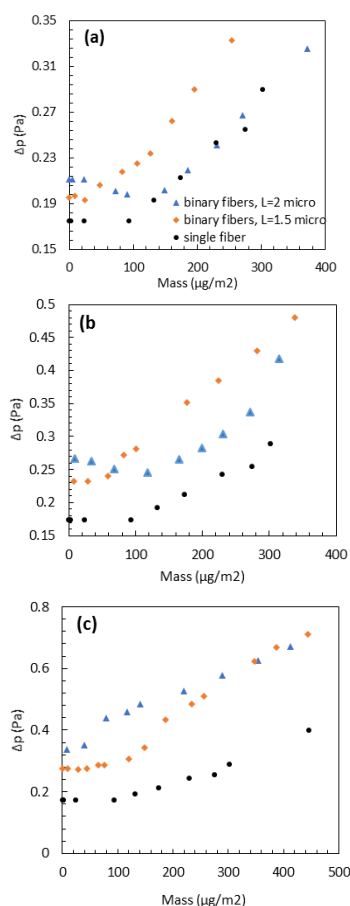
Figures 7 and 8 show the generated pressure drop by different fibers arrangement and fibers distance during particle loading in contrast to the single microfiber, respectively. In Figure 7, the pressure drop is differentially increasing during particle loading. But the value of the pressure drop is different in each fibers arrangement. In the horizontal arrangement of fibers, the

pressure drop is lower, while for the vertical arrangement, it shows a higher value. Generally, in Brownian diffusion, uniform deposition of particles slowly changes the cross section of fiber. Therefore, the rate of increasing of the pressure drop is less than interception mechanism. Also adding a nanofiber to microfiber generates a more resistance for fluid flow than single microfiber at all fiber arrangements.

As shown in Figure 8, the pressure drop increases with the different rate for the single microfiber and fibers arrangement. It can also be seen that the increasing of the pressure drop of binary fibers is similar to the single fiber after 140 $\mu\text{g}/\text{m}^2$  for fibers distance 2  $\mu\text{m}$  at the horizontal arrangement. But for the fiber distance 1.5  $\mu\text{m}$ , the pressure drop increases higher. However, in the cross and vertical arrangement, the pressure drop of binary fibers is higher than single microfiber with fibers distance 1.5 and 2 $\mu\text{m}$ . Because, as it is mentioned before, the deposition of particle upon interception increases the cross section of fibers, which causes higher pressure drop.



**Figure 7.** Pressure drop of different arrangements of binary fibers with fibers distances 1.5 and 2 $\mu\text{m}$  as mass loaded for the particle size 50 nm (a) the horizontal arrangement, (b) the cross arrangement, (c) the vertical arrangement



**Figure 8.** Pressure drop of different arrangements of binary fibers with fibers distance 1.5 and 2 $\mu\text{m}$  as mass loaded for the particle size 150 nm (a) the horizontal arrangement, (b) the cross arrangement, (c) the vertical arrangement

In vertical arrangement, two fibers simultaneously collect particles and form dendrite formation sides of fibers which shows that in this case pressure drop increases higher than other arrangements.

#### 4. CONCLUSION

This study utilized and extended the icoLagrangianFoam solver of open FOAM for the particle capture and growth simulation to investigate the pressure drop and capture efficiency of binary fibers. It was found that the adding of nanofiber to microfiber causes the higher capture efficiency for particle size 50nm at the cross arrangement of binary fibers, while the pressure drop is fairly low and close together for two fiber distances at the cross arrangement. It was demonstrated that the smaller distance of fibers causes more uniformly growth of particles on fibers surface at all fibers arrangement.

For the particle size 150nm, binary fibers have higher capture efficiency than the single microfiber at

all arrangements, especially for the fiber distance 1.5  $\mu\text{m}$ . Generally, a binary system from nano- and microfiber can be effective for obtaining higher capture efficiency upon the interception mechanism at all fiber arrangements. However, the fibers distance should change carefully as it may affect the pressure drop, since a smaller fiber distance causes a higher pressure drop. Therefore, the cross arrangement with the higher capture efficiency and average pressure drop can include a good arrangement to capture the particle size 150 nm with fibers distance 2 $\mu\text{m}$ .

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## Eulerian Lagrangian Simulation of Particle Capture and Dendrite Formation on Binary Fibers

S. Akbarnezhad<sup>a</sup>, A. Soltani Goharrizi<sup>a</sup> M. Salmanzadeh<sup>b</sup>

<sup>a</sup> Department of Chemical Engineering, Shahid Bahonar University of Kerman, Kerman, Iran

<sup>b</sup> Department of Mechanical Engineering, Shahid Bahonar University of Kerman, Kerman, Iran

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بازده جمع آوری ذرات آئروسول خیلی ریز، به شدت تاثیرپذیر از لایه های فیبری است. این مطالعه، نشست و رشد دندریتی ذرات را بر روی آرایش های متفاوت فایبرهایی دوتایی ارائه می کند. شبیه سازی عددی دوبعدی با نرم افزار این فوم انجام شد. نتایج بدست آمده از فرآیند فیلتراسیون لحظه ای، توافق خوبی با مدل سازی موجود دارد. نتایج نشان می دهد که افزودن نانوفایبر به میکروفایبر در آرایش متقاطع از فایبرهای دوتایی با فاصله بین مراکز 2 میکرومتر باعث بازده جمع آوری بزرگتری برای ذرات 50 نانومتر در مقایسه با میکروفایبر منفرد است. برای ذرات بزرگتر 150 نانومتر، بازده و افت فشار در سیستم فایبرهای دوتایی در همه آرایش ها و بویژه برای فاصله بین مراکز 1.5 میکرومتر، بزرگتر از میکرو فایبر منفرد است. بنابراین در اینجا آرایش مناسب از فایبرهای دوتایی برای اندازه ذرات مورد بررسی، آرایش متقاطع با بازده جمع آوری بالا، افت فشار متوسط و فاصله بین مراکز 2 میکرومتر از فایبرها است.

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