



Random Vortex Method for Geometries with Unsolvable Schwarz-Christoffel Formula

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ABSTRACT

In this research we have implemented the Random Vortex Method to calculate velocity fields of fluids inside open cavities in both turbulent and laminar flows. The Random Vortex Method is a CFD method (in both turbulent and laminar fields) which needs the Schwarz-Christoffel transformation formula to map the physical geometry into the upper half plane. In some complex geometries like the flow inside cavity, the Schwarz-Christoffel mapping which transfers the cavity into the upper half plane cannot be achieved easily. In this paper, the mentioned mapping function for a square cavity is obtained numerically. Then, the instantaneous and the average velocity fields are calculated inside the cavity using the RVM. Reynolds numbers for laminar and turbulent flows are 50 and 50000, respectively. In both cases, the velocity distribution of the model is compared with the FLUENT results that the results are very satisfactory. Also, for aspect ratio the cavity (α) equal 2, the same calculation was done for $Re=50$ and 50000. The advantage of this modelling is that for calculation of velocity at any point of the geometry, there is no need to use meshing in all of the flow field and the velocity in a special point can be obtained directly and with no need to the other points.

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NOMENCLATURE

A	Area	z	physical plane	Vectors
F	Schwarz-Christoffel transformation function	Greek Symbols		u Velocity vector
G	Green's function	ζ	Transformation plane	n Unit vector normal to the wall
h	Vortex sheets	η	Gaussian random variable	s Unit vector tangential to the wall
k	Time interval	γ	Circulation per unit length	
p	Pressure	σ	Standard deviation	
Re	Reynolds number	δ	Dirac delta function	
r	radius	Δ	Dilatation	
RVM	Random Vortex Method	∇	Gradient operator	
t	Time	ω	Vorticity	
V	Volume	Γ	Circulation	
W(u,v)	Complex Velocity	ψ	Stream function	

1. INTRODUCTION

Facing the turbulent flows is inevitable in daily life and there is a certain need to study this kind of flows in detail to understand its characteristics [1]. Chorin represented a meshless method to solve the turbulent flows by using the

mathematical equations of the fluid mechanics named the Random Vortex Method (RVM) [2, 3]. This grid-free method is suitable for the analysis of flow at high Reynolds numbers because it has no obvious intrinsic source of diffusion [4]. At two dimensions, Vortex methods generally assign on discretizing vorticity field into a tremendous of vortex blobs [2], which position and intensity establish the underlying velocity field [5]. The proof of convergence was subsequently provided by Beale

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[6] and further improvements in the analysis were given by Cottet [7]. Vortex method was later incorporated into a hybrid vortex-boundary element algorithm for the simulation of viscous flow inside 3-D geometries with moving boundaries of the type found in engines [8].

Methods which rely on vortex methods have achieved extensive popularity recently and have been utilized in a vast range of settings [3, 9-12]. Some early applications have focused on anticipating gross qualitative types of turbulent flow [13-15] and on comparing their results with experiments [16, 17]. Furthermore, numerical precision of the RVM has been studied by [5] for complex flows in laminar and high Reynolds number turbulent flows. Various researches have been performed in the field. H. Shokouhmand et al. [18] used a numerical method to investigate the flow and heat transfer characteristics in a square driven cavity for Reynolds numbers from 1 to 10000. M. Taghilou et al. [19] used the single relaxation time (SRT) lattice Boltzmann equation to simulate lid driven cavity flow at different Reynolds numbers (100-5000). Their investigation showed that with increasing the Reynolds number, bottom corner vortices will grow but they won't merge together. In addition, the merger of the bottom corner vortices into a primary vortex and creation of other secondary vortices was shown in the cases which the aspect ratios are bigger than one. B. Zafarmand and coworkers [20] studied turbulent flow in a channel using Vortex Blob Method (VBM) and obtained physical concepts of turbulence. In their work, time-averaged velocities, and then their fluctuations are calculated. M. Taghilou et al. [19] used the SRT lattice Boltzmann equation to simulate lid driven cavity flow at different Reynolds numbers (100-5000) and three aspect ratios, $K=1, 1.5$ and 4 .

The main reason that meshless methods are significantly interested is that the well-established and successful numerical methods like the finite volume/finite elements need a mesh. The automatic generation of a high quality mesh poses a serious problem in the analysis of practical engineering systems. Furthermore, the analysis and simulation of certain types of problems (like dynamic crack propagation) require an expensive remeshing operation. Meshless methods overcome these problems associated with meshing by eliminating the mesh altogether [21].

In this research we obtain the angels of Schwarz-Christoffel transformation mapping with numerical method, then use the mapping in the Random Vortex Method to calculate turbulent and laminar flow field inside square and rectangular open cavities by the Random Vortex Method.

2. NUMERICAL SCHEME

2.1 Formulation Navier-Stokes and continuity equations, due to the vorticity-most important aspect of turbulence- and vortex stretching effects in the two

dimensional formulation, will be simplified to

$$Du / Dt = \text{Re}^{-1} \nabla^2 \mathbf{u} - \nabla p \quad (1)$$

Here, Re plays the role of Reynolds number at inlet of the system and $\mathbf{u}=(u,v)$ signifies the velocity which is normalized, p is the normalized pressure and ∇ shows the gradient operator, ∇^2 expresses the Laplacian, and $\frac{Du}{Dt} = \frac{\partial}{\partial t} + \mathbf{u} \cdot \nabla$ implies the substantial derivative.

By solving these equations considering the boundary conditions, the flow field is specified

$$\text{at inlet} \quad \mathbf{u} = (1,0) \quad (2)$$

$$\text{On the walls} \quad \mathbf{u} = 0 \quad (3)$$

As we know, the second element of the flow field is vorticity

$$\omega = \nabla \times \mathbf{u} \quad (4)$$

Then:

$$D\omega / Dt = \text{Re}^{-1} \nabla^2 \omega \quad (5)$$

$\mathbf{u}(\mathbf{r})$ will be achieved by (1) and (4), when (5) is utilized for updating $\omega(\mathbf{x}, y)$ - the field of vorticity.

Based on the Helmholtz's Theorem [2, 16] the mechanism of momentum transport, is revealed by a synthetic method of approach, velocity decomposition theorem (known also as the Hodge decomposition), that plays a vital role in contemporary computational fluid mechanics. According to Helmholtz's Theorem, the velocity vector is discretized into a divergence-free, irrotational, rotational and curl-free components i.e.

$$\mathbf{u} = \mathbf{u}_\omega + \mathbf{u}_\Delta \quad (6)$$

$$\text{where} \quad \nabla \cdot \mathbf{u}_\omega \equiv 0 \quad (7)$$

$$\text{while} \quad \nabla \times \mathbf{u}_\Delta \equiv 0 \quad (8)$$

Both the components of mentioned velocity need to satisfy the boundary conditions of zero normal velocity,

$$\mathbf{u}_\omega \cdot \mathbf{n} = 0 \text{ and } \mathbf{u}_\Delta \cdot \mathbf{n} = 0 \quad (9)$$

while, \mathbf{n} is the unit vector normal to the walls and \mathbf{u} -the total velocity- has to satisfy the no-slip boundary condition

$$\mathbf{u} \cdot \mathbf{s} = 0 \quad (10)$$

where, \mathbf{s} signifies the unit vector which is tangential to the walls [2].

2.1.1. Vortex Dynamics What is named vortex blob signifies ω_j -a discrete elementary vorticity- which its acting domain is ΔV_j -an elementary volume- located at \mathbf{r}_j . Its intensity is calculated with the Dirac delta function, i.e.

[2, 4, 22]

$$\omega_j = \Gamma_j \delta(r - r_j) \tag{11}$$

where,

$$\Gamma_j = \lim_{\Delta V_j \rightarrow 0} \int_{\Delta V_j} \omega_j dV \tag{12}$$

is its local circulation.

By Dirac delta and approaching ΔA_j to zero and using Green function, we will have:

$$\psi(x) = \sum_j G_j \Gamma_j \tag{13}$$

For which,

$$\Gamma_j = \int_{\Delta A_j} \omega_j dA \tag{14}$$

Finally, by definition of Equation (1), in terms of complex variables we will have

$$w_\psi(z, z_j) = \frac{-i \Gamma_j |z - z_j|}{2\pi \max(|z - z_j|, r_o)} \frac{1}{z - z_j} \tag{15}$$

while w implies the velocity at physical plane and $z = x + iy$ and r_o is the cut-off radius, where velocity is constant.

Velocity fields satisfying boundary conditions, $u_\omega \cdot n = 0$ and $u_\Delta \cdot n = 0$, can be achieved using any Poisson solver. For the Random Vortex Method we use the classical method of conformal mapping, which transforms the velocity field into the upper-half plane (ζ -plane).

Then:

$$w_\omega(\zeta, \zeta_j) = w_\psi(\zeta, \zeta_j) - w_\psi(\zeta, \zeta_j^*) \tag{16}$$

Using Equation (4), $w(\zeta, \zeta_j)$ will be achieved. Asterisk is complex conjugate. Consequently, the velocity field affected by vortex blobs will be:

$$w_\omega(\zeta) = w_p(\zeta) + \sum_{j=1}^{j_s} w_\omega(\zeta, \zeta_j) \tag{17}$$

By using the Schwarz-Christoffel conformal mapping, the transformation function will be:

$$F(\zeta) = d\zeta / dz \tag{18}$$

while

$$w(z) = w(\zeta) F(\zeta) \tag{19}$$

is the velocity vector in forms of complex variable.

Displacing of vortex elements with diffusion

mechanism will occur by two (perpendicular directions) independent-Gaussian random with mean of zero and standard deviation of $\sigma = (2k/Re)^{1/2}$.

Displacement by combination of the two mentioned mechanisms will occur:

$$z_j(t+k) = z_j(t) + w^*(z_j)k + \eta_j \tag{20}$$

while, $\eta_j = \eta_{xs} + i \eta_{ys}$, and $w = w_\omega + w_\Delta$ or, in upper-half plane:

$$\zeta_j(t+k) = \zeta_j(t) + w^*(\zeta_j) F^*(\zeta_j) F(\zeta_j)k + (\eta_j) F(\zeta_j) \tag{21}$$

Using (21) is simpler than (20) and more direct and the velocity field in transform-plane will be calculated by (17).

w needs to be obtained at points along the wall to satisfy the no-slip boundary condition. Distance between these points is considered as h along walls of geometry. As we know, the tangential velocity at walls is not zero, thus, a vortex is created with a circulation of $h \cdot u_w$ to satisfy this condition. Due to loss of vortexes near walls because of diffusion, accuracy is poor near solid walls. Furthermore, inside blob cores, velocity is assumed to be constant, and gradient of velocity near solid surfaces are too high. To overcome this problem, introduction of vortex sheets near walls is necessary [2, 4, 22].

2. 1. 2. Vortex Sheets To satisfy no-slip boundary condition, w needs to be obtained at points along the wall. For achieving this purpose Chorin [3] introduced a thin numerical shear layer where the effects of vortex sheets overcome the blobs. In this section, the two undermentioned conditions is established:

I $\partial v / \partial x \ll \partial u / \partial y$

II Diffusion is negligible in comparison to convection in the x-direction

For mentioned sheets, (1) is reduced to

$$\omega_\delta = -\partial u / \partial y \tag{22}$$

Then, $u_\omega(r)$ -the velocity vector- inside the sheer layer, needs to be calculated:

$$u_\delta(x) - u(x_i, y_i) = -\int_{y_i}^{\delta_s} \omega dy \tag{23}$$

where, δ_s is outside boundary of the shear layer and y_i the calculation point. Considering $u_\delta = u$ at $y = \delta$, the integral of (23) is converted to a summation. Then

$$\gamma_j = \lim_{\Delta y \rightarrow 0} \int_{y_i}^{y_i + \Delta y} \omega dy \tag{24}$$

where, (24) is the circulation of each unit of a vortex sheet. Then, the circulation of each vortex sheet by length of h :

$$\Gamma_j = h \times \gamma_j \tag{25}$$

Then, the velocity difference across length of any unit is

$$\Delta u_j = \gamma_j \tag{26}$$

As a consequence of (23), the effectiveness zone of a vortex sheet is limited to a 'shadow' below it.

Thus:

$$u(x_i, y_i) = u_\delta(x_i) - \sum_j \gamma_j d_j \tag{27}$$

while,

$$d_j = 1 - |x_i - x_j| / h \tag{28}$$

According to Helmholtz theorem, the normal velocity:

$$v = -\partial I / \partial x \tag{29}$$

while,

$$I = \int_0^{y_i} u dy = u(x_i) y_i - \int_0^{y_i} y du = u(x_i) y_i - \sum_j \gamma_j d_j y_j \tag{30}$$

(29) is converted to (31) by finite-difference

$$v(x_i - y_i) = -\{I^+ - I^-\} / h \tag{31}$$

while, according to (30),

$$I^\pm = u_\delta(x_i \pm \frac{1}{2}h) y_i - \sum_j y_j^0 \gamma_j d_j^\pm \tag{32}$$

And

$$d_j^\pm = 1 - (x_i \pm \frac{1}{2}h - x_j) / h \tag{33}$$

and $y^0 = \min\{y_i, y_j\}$

Diffusion mechanism of a sheet is $\eta_i = 0 + i\eta_y$, considering condition II. The item $-1/2\gamma_j$ is used to match vortex sheets motion with vortex blobs and effect of their image [2, 4, 22].

2. 2. Algorithm

By adopting time step (k), according to Courant condition which says that $k \leq h/\max u$ [4] and h -the strength of the sheet which specifies their spatial resolution, calculations are started. σ -the standard deviation- is identified for a given Reynolds number. Then, sheets number needs to be chosen considering γ value. These mentioned items are equivalent to items which are made in corresponding step and a grid size in a finite difference algorithm.

The initial conditions is the potential flow which is obtained by solution of $\nabla^2 \psi = -\omega$.

To stay with condition of no boundary, the core radius (r_o) is fixed. By setting $r_o > \delta_s$ error of this requirement will

tend to zero. The potential velocity, created by a vortex blob is obtained at the wall, according to (25)

$$u_o = \Gamma_j / \pi r_o \tag{34}$$

while, considering (26) with $\Delta u_j = u_o$,

$$r_o = h / \pi \tag{35}$$

This equation provides relation between the core radius and the vortex sheet length.

Using equations (20), (27) and (31), vortex sheets move in shear layer. After calculation of sheets displacement, new location of sheets needs to be considered. A sheet which jumps out of the shear layer, has two possible location. If it jumps into the geometry, it converts to a vortex blob. If it jumps out of the geometry, but inside the shear layer image, it will be a sheet with previous location inside the shear layer, otherwise it will be removed. For minimizing losing of a blob, the condition of $\delta_s < r_o$ has to be considered.

3. IMPLEMENTATION

As mentioned above, we need the Schwarz-Christoffel formula for our geometry. Our geometry is an open cavity,

then $F(\zeta) = \sqrt{(\zeta^2 - a^2) / (\zeta^2 - b^2)}$.

a & b are the corners at the z plane which are transformed to the ζ plane. For the open cavity F(ζ) is not solvable, hence a and b are obtained as follow:

We find a and b by using the Runge-Kutta 4th code. As we see in Figure 1, (0,0) at the physical plane is transformed to (0,0) at the ζ plane. We use this node to find a and b. At first we assume that B (0.5,1) is transformed to b (1,0). A=(0.5,0) and $F(\zeta) = d\zeta / dz$ then

$d\zeta / dz = \sqrt{(\zeta^2 - a^2) / (\zeta^2 - b^2)}$, therefore we need to find

the angle "a" to have F(ζ). As shown in Figure 2, we change assumed a, until the residual becomes constant.

Residuals = abs[(assumed a-obtained a) / a].

Then, having the new a, we go to find b, and so on. Finally, a and b are obtained.

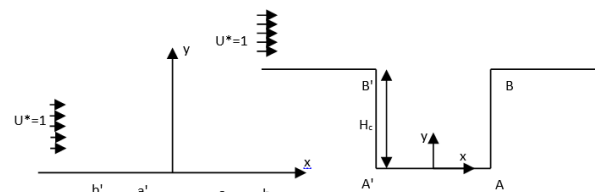


Figure 1. (Left): Schwarz-Christoffel ζ plane; (right): Schwarz-Christoffel z(physical) plane

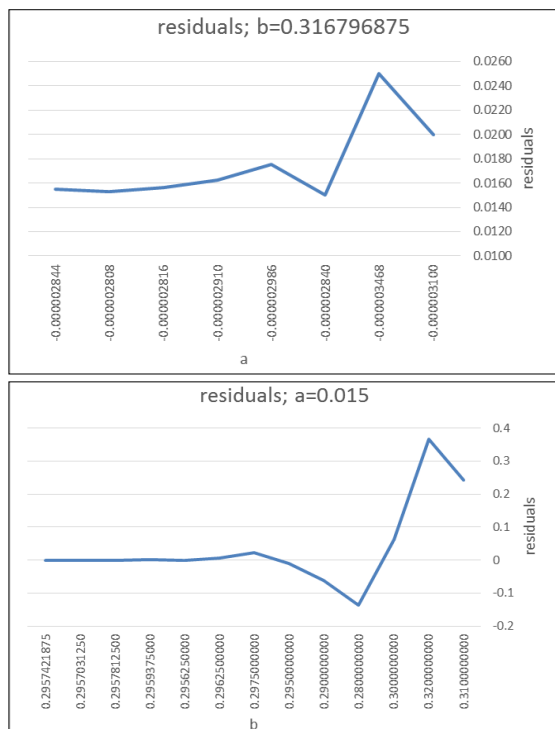


Figure 2. Convergence of calculation of a and b for $\alpha=1$

4. CONVERGENCE

As mentioned before, to obtain one angle, another angle is guessed and by using the Runge-Kutta 4th code another angle is obtained. Then, the residual is calculated. After the first guessed angle is changed by adding slightly and again, second new angle is obtained.

As it can be observed from Figure 2, calculations continue until the residual reaches just around zero. In all graphs of the Figure 2, convergence is obvious.

5. RESULTS AND DISCUSSION

First, the code was written for a square cavity with the Reynolds number of 50. To compare our results, the FLUENT was used and the conformity was satisfactory. In the foregoing flow, the dimensionless velocity, u , plotted at the center line of the cavity and compared with the result of the FLUENT (Figure 3), which the agreement was perfect. The code was changed for the Reynolds number of 50000.

All of the parameters used in our code are listed in Table 1.

Formation of the primary eddy at the cavity center was observed (Figure 4). The primary eddy's center was formed perfectly at the cavity's center. In addition to formation of the two secondary eddies at the bottom of the cavity, there was another small eddy at the top left.

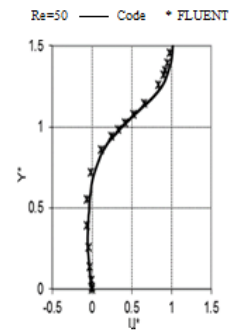


Figure 3. Average u velocity at centerline of cavity, (*) FLUENT, (-) code, at (Re=50 & $\alpha=1$)

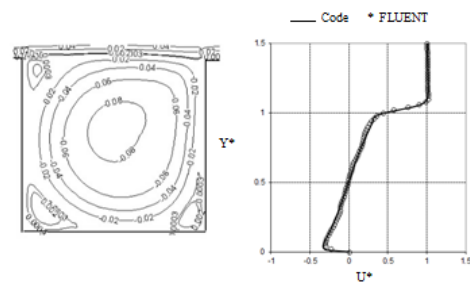


Figure 4. (Left): Stream lines of code, at Re= 50000 & $\alpha=1$; (Right): average u velocity at centerline of cavity, (o) FLUENT, (-) code, at Re=50000

TABLE 1. Numerical parameters used in code

Reynolds number	50	50000
Δt (k)	0.05	0.05
h	0.2	0.05
$\Delta x = \Delta y$	0.02	0.02
Y_s	1.4σ	2σ
Iterations	70	500
It.s for average vel.	20	300
Total iterations	90	800

Also, at this Reynolds number, the average velocity, u , was plotted at the center line of the cavity and compared with the FLUENT (Figure 4-right). In this condition, the coincidence was very good. The $K-\omega$ method was used for the turbulent flow and the convergence of the FLUENT results reached after 8000 iteration with residuals of $k=0.5 \times 10^{-4}$, $\omega=1 \times 10^{-4}$, continuity= 0.5×10^{-5} and $xvel. \& yvel. = 1 \times 10^{-6}$.

We need to point out that the velocity measures and streamlines, which are plotted in Figure 4, are average; therefore, to see the instantaneous status, instantaneous u velocity at centerline of cavity has been plotted in Figure 5. As seen in the figure, the velocity has fluctuations which are one of turbulent flows specification.

In this figure, the instantaneous streamlines contours are shown as well. As noted, the contours do not have any regular shape which is another specification of turbulent flows. Incidentally, all primary and three secondary eddies are formed at the moment but have an irregular shape. As we know, having velocity fluctuations, Reynolds stresses can be obtained.

Also, for the cavity aspect ratio (α) equal 2, the same calculation was done for $Re=50$ and 50000 . Figures 6 and 7 demonstrate both the streamlines and comparison of the velocities center line obtained by the model and by the FLUENT. An acceptable agreement is observed.

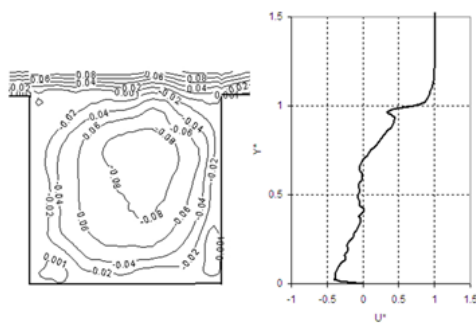


Figure 5. (Left): Instantaneous stream lines of code; (Right): instantaneous u velocity of code at center line of cavity ($Re=50000$ & $\alpha=1$)

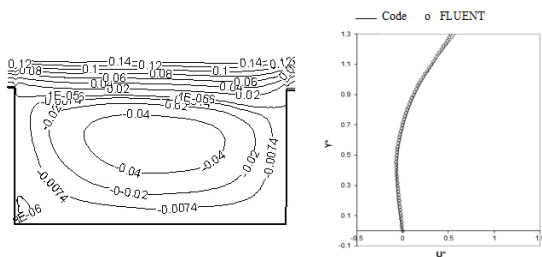


Figure 6. (Left): Stream lines of code, at $Re= 50$ & $\alpha=2$; (Right): average u velocity at centerline of cavity, (o) FLUENT, (-) code, at $Re=50000$

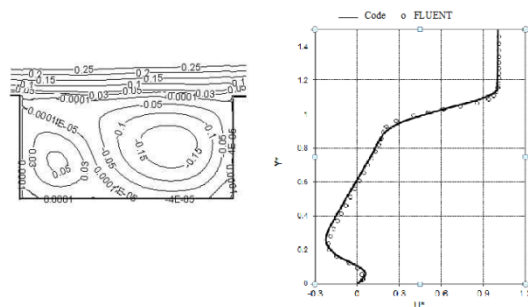


Figure 7. (Left): Stream lines of code, at $Re= 50000$ & $\alpha=2$; (Right): average u velocity at centerline of cavity, (o) FLUENT, (-) code, at $Re=50000$

6. CONCLUSION

A method to determine angles of the Schwarz-Christoffel mapping formula which is used in the Random Vortex Method is studied. Then, a code is written by RVM for an open square cavity and formation eddies is investigated in laminar and turbulent flows. Furthermore, dimensionless velocity at centerline of cavity is compared by FLUENT results. By using appropriate parameters, RVM is a very successful method in studying two-dimensional, viscous, incompressible and time dependent flows. Having instantaneous velocities, velocity fluctuations are achievable; consequently, Reynolds stresses can be calculated. Flow field -obtained by the Random Vortex Method- can be utilized in studying heat transfer and many other applications.

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Random Vortex Method

Turbulent

در این تحقیق از روش گردابه‌های تصادفی برای محاسبه میدان سرعت جریان در داخل حفره‌های باز برای جریان آرام و درهم استفاده شده است. روش گردابه‌های تصادفی یک روش محاسباتی است (در هر دو میدان آرام و درهم) که جهت انتقال هندسه به نیم‌صفحه بالایی، از نگاشت Schwarz-Christoffel استفاده می‌کند. در برخی از هندسه‌های پیچیده مانند جریان داخل حفره، نگاشتی که هندسه را به نیم‌صفحه بالایی منتقل می‌کند به آسانی به دست نمی‌آید. در این مقاله تابع انتقال مذکور برای حفره مربعی و مستطیلی (با نسبت طول به عرض ۲) به صورت عددی به دست می‌آید. سپس، میدان‌های سرعت لحظه‌ای و متوسط داخل حفره توسط روش گردابه‌های تصادفی محاسبه می‌شوند. اعداد رینولدز برای جریان‌های آرام و درهم به ترتیب ۵۰ و ۵۰۰۰۰ است. در هر دو مورد، توزیع سرعت مدل با نتایج فلوننت مقایسه می‌شود که بسیار رضایت بخش هستند. مزیت این روش مدل سازی اینست که برای محاسبه سرعت در هر نقطه از هندسه، احتیاجی به مش بندی در کل میدان جریان نبوده و سرعت در یک نقطه خاص می‌تواند مستقیم و بدون وابستگی به نقاط دیگر به دست آید.

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